# Extracting carbon from seawater

### *Indirect CO<sub>2</sub> capture*

**Vojtech Konderla David Vermaas**

**15th December 2022**





# Driving force



# Driving force

 $\widetilde{\mathbf{T}}$ UDelft



How can we reach carbon-neutral society when we are still using fossil fuels?



3 *[1] European Environment Agency, https://www.eea.europa.eu/data-and-maps/data/data-viewers/greenhouse-gases-viewer [2] EU vision on 'Going Climate-neutral in 2050*

# Driving force



*Batteries instead of jet fuel? Biomass instead of petrochemicals?*

We need negative  $CO<sub>2</sub>$  emission technology

*Renewable energy sources and process intensification are both not good enough*

How can we reach carbon-neutral society when we are still using fossil fuels?





 $\widetilde{\mathbf{T}}$ UDelft

*[1] European Environment Agency, https://www.eea.europa.eu/data-and-maps/data/data-viewers/greenhouse-gases-viewer [2] EU vision on 'Going Climate-neutral in 2050*

### Carbon cycle





### Carbon cycle





#### Flue gas



**Negative emission in** combination with biomass



Flue gas Air



**Negative emission in** combination with biomass



**Needs to filter full** atmosphere each 35 years





**Negative emission in** combination with biomass



**Needs to filter full** atmosphere each 35 years

Flue gas Air Air Seawater



- **Concentration 150x higher** than in air
- **Lower TRL than air capture**



# Where is our  $CO<sub>2</sub>$ ?



*[1]*

Flue gas Air



**Negative emission in** combination with biomass

**UDelft** 



**Needs to filter full** atmosphere each 35 years

#### Seawater



- **Concentration 150x higher** than in air
- **Lower TRL than air capture**

*using:*

#### Electrochemical methods

- **Direct use of electricity**
- **Modular**
- **I**sothermal

11

# Atmosphere and ocean are in equilibrium





# Atmosphere and ocean are in equilibrium



*Removing CO<sub>2</sub> from the ocean* means removing CO<sub>2</sub> *indirectly from the air*



### Seawater carbon capture – pH swing



 $\widetilde{\mathbf{T}}$ l

**UDelft** 

 $H^+ + HCO_3^- \leftrightarrow CO_2 + H_2O$  $HCO_3^- + OH^- \leftrightarrow CO_3^{2-} + H_2O$ 

### Seawater carbon capture – pH swing



 $DIC = [CO_{2,(aq)}] + [HCO<sub>3</sub><sup>-</sup>] + [CO<sub>3</sub><sup>2</sup> -]$ 

**UDelft** 

#### pH swing can be achieved by

- Water electrolysis
- Redox active carriers
- Bipolar membranes

...

 $H^+ + HCO_3^- \leftrightarrow CO_2 + H_2O$  $HCO_3^- + OH^- \leftrightarrow CO_3^{2-} + H_2O$ 

### Seawater carbon capture – pH swing



 $DIC = [CO_{2,(aq)}] + [HCO<sub>3</sub><sup>-</sup>] + [CO<sub>3</sub><sup>2</sup> -]$ 

 $\widetilde{\mathbf{T}}$ UDelft





 $H^+ + HCO_3^- \leftrightarrow CO_2 + H_2O$  $HCO_3^- + OH^- \leftrightarrow CO_3^{2-} + H_2O$ 

16

### 3 compartment Bipolar Membrane Electrodialysis (BPMED)





# 3 compartment Bipolar Membrane Electrodialysis (BPMED)



**UDelft** 



# 3 compartment Bipolar Membrane Electrodialysis (BPMED)





# Aspen modeling results

**•** Results are scaled up for the size of the desalination plant  $\sim$  137 kg/h CO<sub>2</sub>, 177 kg/h CaCO<sub>3</sub>





# Aspen modeling results

**• Results are scaled up for the size of the desalination plant**  $\sim$  **137 kg/h CO2, 177 kg/h calcite** 



Power consumption *=f(current density)*



Number of stacks *=f(current density)*



# Total power consumption



■ Sum of the electrochemical and pumping power

#### CO<sub>2</sub> energy consumption:

- **3 comp.:** 249 kJ/mol
- **2 comp.:** 303 kJ/mol
- Digdaya *et al.* 2020: 155 kJ/mol[1],\*
- Eisaman *et al.* 2012: 242 kJ/mol[2],\*

#### **CO2 & CaCO3 energy consumption**

- **3 comp.:** 158 kJ/mol
- **2 comp.:** 193 kJ/mol
- Results are scaled up for the size of the desalination plant  $\sim$  137 kg/h CO<sub>2</sub>, 177 kg/h CaCO<sub>3</sub>



*\* Does not include pumping power, considers regular seawater*

*[1] Digdaya, I.A., Sullivan, I., Lin, M. et al. A direct coupled electrochemical system for capture and conversion of CO2 from oceanwater. Nat Commun 11, 4412 (2020) [2] Eisaman, M. & Parajuly, Keshav & Tuganov, Alexander & Eldershaw, Craig & Chang, Norine & Littau, Karl. (2012). CO2 extraction from seawater using bipolar membrane electrodialysis. Energy Environ. Sci.. 5. 10.1039/C2EE03393C.* 

# Total power consumption

- **Natural gas:** 400 kJ/mol *electricity/CO<sub>2</sub>*
- **Thermodynamic minimum: 20 kJ/mollengler**

▪ Sum of the electrochemical and pumping power

#### CO<sub>2</sub> energy consumption:

- **3 comp.:** 249 kJ/mol
- **2 comp.:** 303 kJ/mol
- Digdaya *et al.* 2020: 155 kJ/mol[1],\*
- Eisaman *et al.* 2012: 242 kJ/mol[2],\*

#### **CO2 & CaCO3 energy consumption**

- **3 comp.:** 158 kJ/mol
- **2 comp.:** 193 kJ/mol
- Results are scaled up for the size of the desalination plant  $\sim$  137 kg/h CO<sub>2</sub>, 177 kg/h CaCO<sub>3</sub>



*\* Does not include pumping power, considers regular seawater [1] Digdaya, I.A., Sullivan, I., Lin, M. et al. A direct coupled electrochemical system for capture and conversion of CO2 from oceanwater. Nat Commun 11, 4412 (2020) [2] Eisaman, M. & Parajuly, Keshav & Tuganov, Alexander & Eldershaw, Craig & Chang, Norine & Littau, Karl. (2012). CO2 extraction from seawater using bipolar membrane electrodialysis. Energy Environ. Sci.. 5. 10.1039/C2EE03393C.* 

# BPM limits the energy consumption

BPM thermodynamic voltage:  $V_{BPM} = 0.059 \Delta pH_{BPM}$ , however, in practice water splitting starts only at 0.6V



*In-situ* CaCO<sub>3</sub> mineralization using 2 compartment BPMED with 10 BPMs

# BPM limits the energy consumption

Del

BPM thermodynamic voltage:  $V_{BPM} = 0.059 \Delta pH_{BPM}$ , however, in practice water splitting starts only at 0.6V





- BPM consumes approximately 90% of the electrical energy
- $\triangleright$  Market for BPMs is still in early stages
- Water splitting catalyst inside the BPM needs to be improved

*[1] Sharifian, R., et al. "Oceanic carbon capture through electrochemically induced in situ carbonate mineralization using bipolar membrane." Chemical Engineering Journal 438 (2022) [2]* Blommaert, Marijn A., et al. "Insights and challenges for applying bipolar membranes in advanced electrochemical energy systems." *ACS Energy Letters* 6.7 (2021)

# Number of BPMED stacks





*,where 1 cell stack contains 210 compartments with 0.5x0.5 m2 active area*

Results are scaled up for the size of the desalination plant  $\sim$  137 kg/h CO<sub>2</sub>, 177 kg/h CaCO<sub>3</sub>

#### ▪ **3 comp.:**

- **Design requires an additional dilute compartments**
- 210 compartments stack corresponds to a pilot scale stack developed at AquaBattery

# 3 compartment Bipolar Membrane Electrodialysis



 $\widetilde{\mathbf{T}}$ UDelft





### Conclusion – challenges to overcome

- Cost-efficient renewable electricity (Fluctuations are alright)
- **Finding Suitable coastal location(s)** : operation (ocean movements, carbon cycle) but also  $CO<sub>2.00</sub>$  storage
- Monitoring, reporting and verifying (MRV): Effect on ecosystem + geography
- **Technology: fouling, pumping, pretreatment, low TRL, LCA**
- Upscaling: Permit(s), Funding



### Dutch Indirect Carbon Capture start-up





**Ir. Vojtech Konderla** TU Delft Research engineer

 $\widetilde{\mathbf{T}}$ UDelft



**Dr. Ir. David A. Vermaas** TU Delft associate professor



**Ruben Brands (MBA & LL.M)** Business & corporate law



**Dr. Ir. Rose Sharifian** Former TU Delft PhD



# Upscaling and future view



